

U.S. EPA Hardrock Mining Conference 2012 (Advancing Solutions for a New Legacy)

“ARD REMEDIATION WITH SLAG: AN APPLICATION TO BERKELEY PITLAKE WATER”

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Outline

- **Berkeley Pitlake**
- **Previous Research**
- **Silicate Slags**
- **Objectives**
- **Procedures**
- **Results & Discussions**
- **Conclusions**
- **Acknowledgements**

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Interstate-15

tailings pond

road

Continental Pit

terraces

tailings

Treatment Plant

Horseshoe Bend Water

Berkeley Pit

MR Concentrator

Viewing Stand

Butte

Walkerville

Interstate 15/90





Brief History of Berkeley Pit

- 1880 - Butte was an early copper-mining town:
 - Referred to as “The Richest Hill on Earth”
 - One of the world’s largest sulfide ore deposits
- 1920 - ACC controlled most mines
- 1955 - ACC began phasing out underground mining
- 1977 - ARCO purchased all operations
- 1982 - Operations halted and pumps turned off
- 1983 - Water first appeared in the pit
 - Listed as a Superfund site
 - Part of the largest mining Superfund site



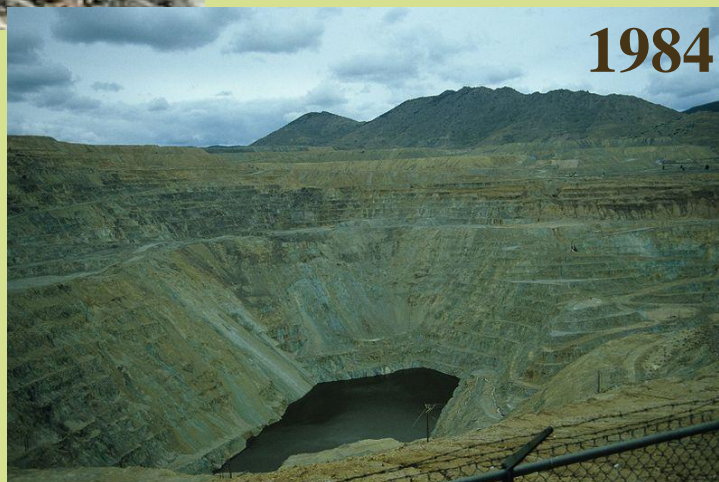
1979

Berkeley Pitlake Water:

- **is acidic near pH 2.5**
- contains metals at high concentrations (99% Water):

SO ₄	(7500 ppm)
Fe	(1000 ppm)
Zn	(650 ppm)
Al	(300 ppm)
Mn	(250 ppm)
Cu	(200 ppm)
Cd	(2.5 ppm)
As	(0.5 ppm)

Concentrations change with position, depth and time



1984

Berkeley Pitlake Water:

- encompasses ~700 acres
- **is ~1,000 feet deep**
- contains ~40 billion gallons
- **fills at 2.6 million gallons per day**
- will reach “critical level” in 2023



1995

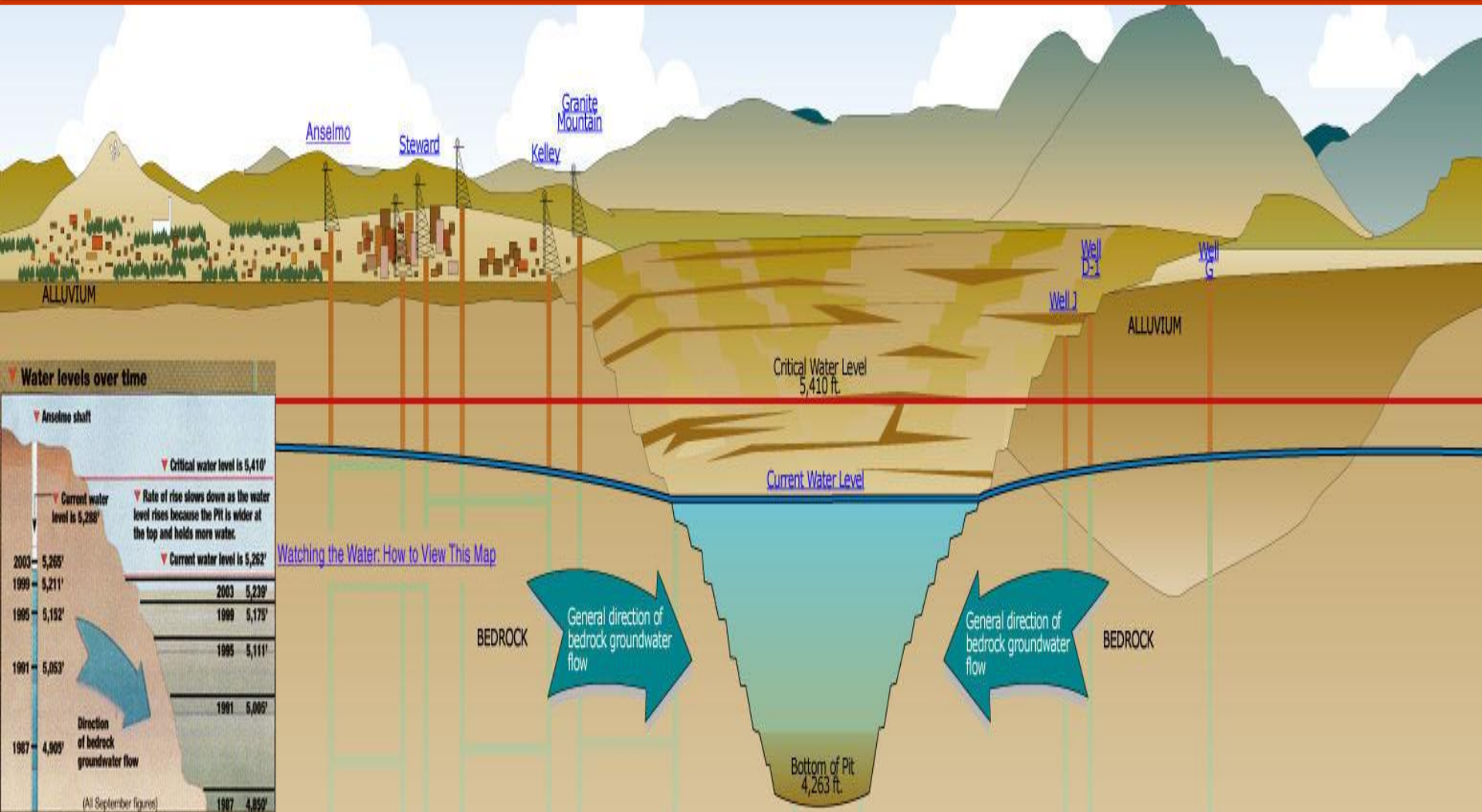


– Continental Pit –

Critical Water Level

– Horseshoe Bend Water

Monitoring the Water Level



Brief History of Berkeley Pit

- 1995 - HSBW also diverted to pond (3M GPD)
 - MR starts operating Continental Pit to the east
 - ARCO and MR named responsible parties
- 2000 - MR halts operations including diversion
- 2003 - HSBW Treatment Plant is commissioned
 - two-stage lime precipitation process
 - diversion of treated water begins
 - sludges are disposed into the BPL
- 2004 - MR reopens and begins full operations
- 2005 - MR pumps BPL water to Cu-cementation

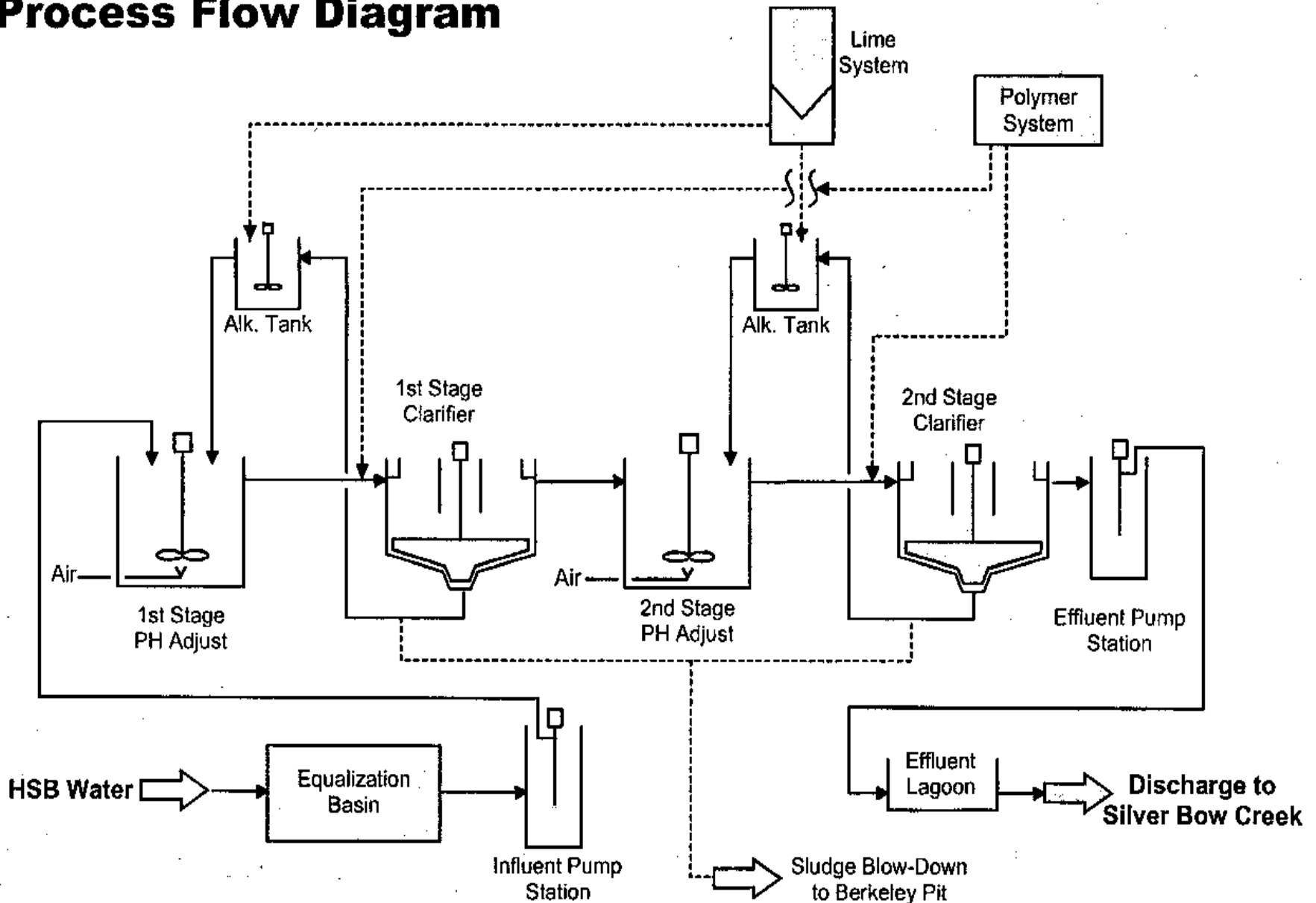


Horseshoe Bend Water Treatment Plant



Horseshoe Bend Water Treatment Plant

ARCO / Montana Resources Horseshoe Bend Water Treatment Facility Process Flow Diagram



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Previous Research

- **Participate in a “series” of 5 studies to summarize available information**
- **Generate new information to formulate conceptual environmental models for the Berkeley Pitlake from all of its features**
- **Provide data for the development of advanced treatment technologies**

Series I – Selective Recovery

	Fe	As	Mn	Cu	Cd	Zn	Al
Initial BPL Water	1019.8	5.9	214.2	151.2	2.3	566.3	243.5
Stage 1A - H ₂ O ₂ /UV	8.43	< 0.11	198.5	146.3	1.9	529.7	222.7
Stage 1B - KMnO ₄	0.23	< 0.11	4.5	138.8	1.84	495.6	213.2
Stage 2 - Na ₂ S	0.27	< 0.11	4.9	0.09	1.7	482.6	203.2
Stage 3 - Na ₂ S	0.22	< 0.11	4.2	< 0.05	< 0.02	49.4	186.2
Stage 4 - NaOH	< 0.04	< 0.11	3.72	< 0.05	< 0.02	18.2	0.24
Drinking Standard	0.3	0.05	0.05	1.3	0.005	5	0.2

Stage 1A: $\text{H}_2\text{O}_2 = 2\text{OH}^\bullet$; $\text{Fe}^{2+} + \text{OH}^\bullet = \text{Fe}^{3+} + \text{OH}^-$; $\text{Fe}^{3+} + 3\text{OH}^- = \text{Fe}(\text{OH})_3$

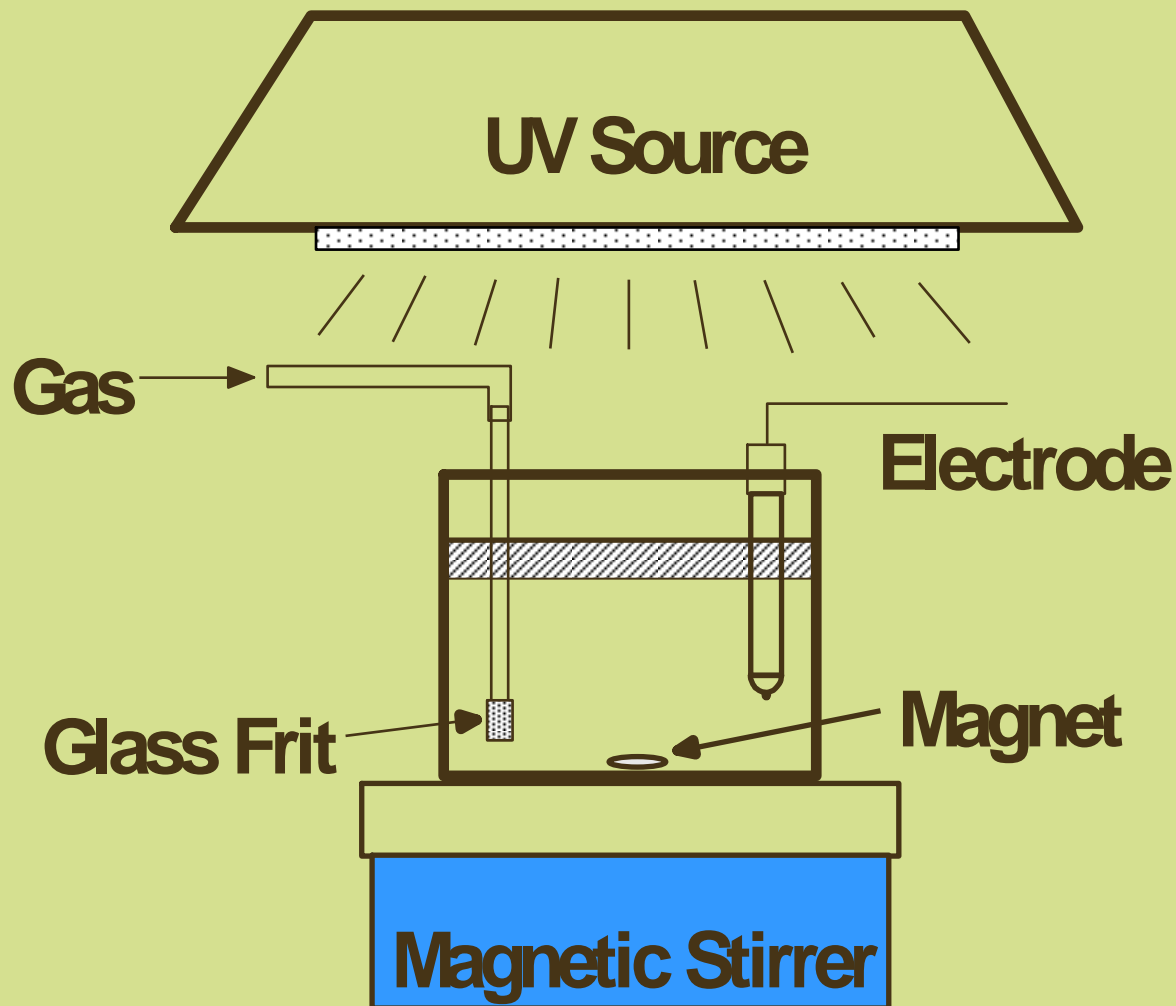
Stage 1B: $3\text{Mn}^{2+} + 2\text{MnO}_4^- + 2\text{H}_2\text{O} = 5\text{MnO}_2 + 4\text{H}^+$

Stage 2: $\text{Cu}^{2+} + \text{S}^{2-} = \text{CuS}$

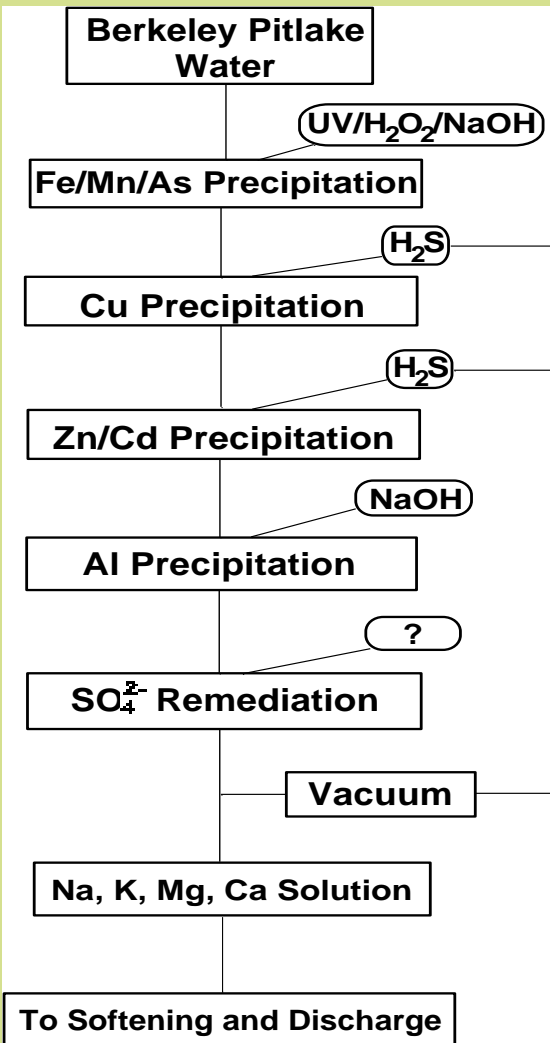
Stage 3: $\text{Cd}^{2+} + \text{S}^{2-} = \text{CdS}$; $\text{Zn}^{2+} + \text{S}^{2-} = \text{ZnS}$

Stage 4: $\text{Al}^{3+} + 3\text{OH}^- = \text{Al}(\text{OH})_3$

Series I – Selective Recovery

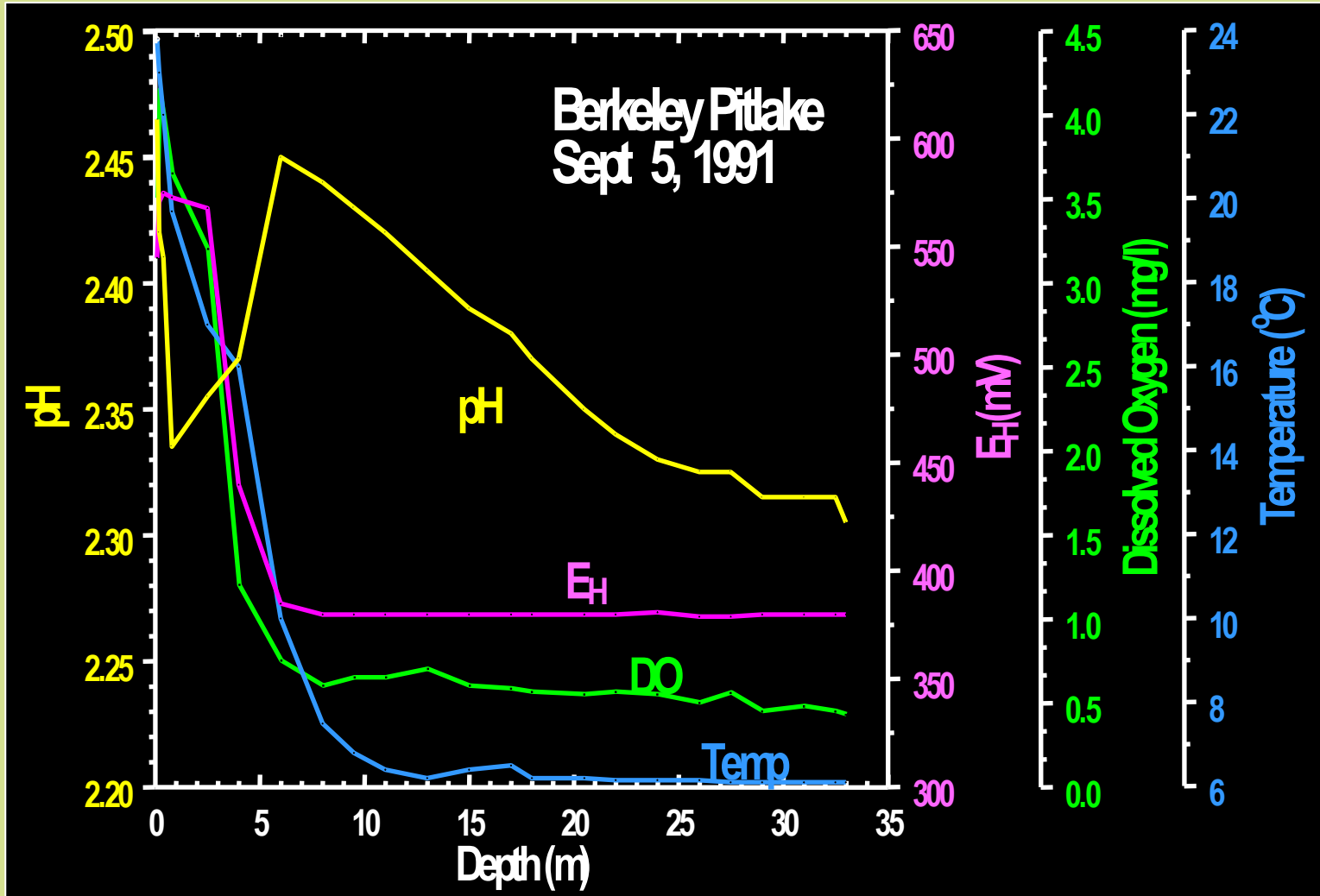


Series I – Selective Recovery

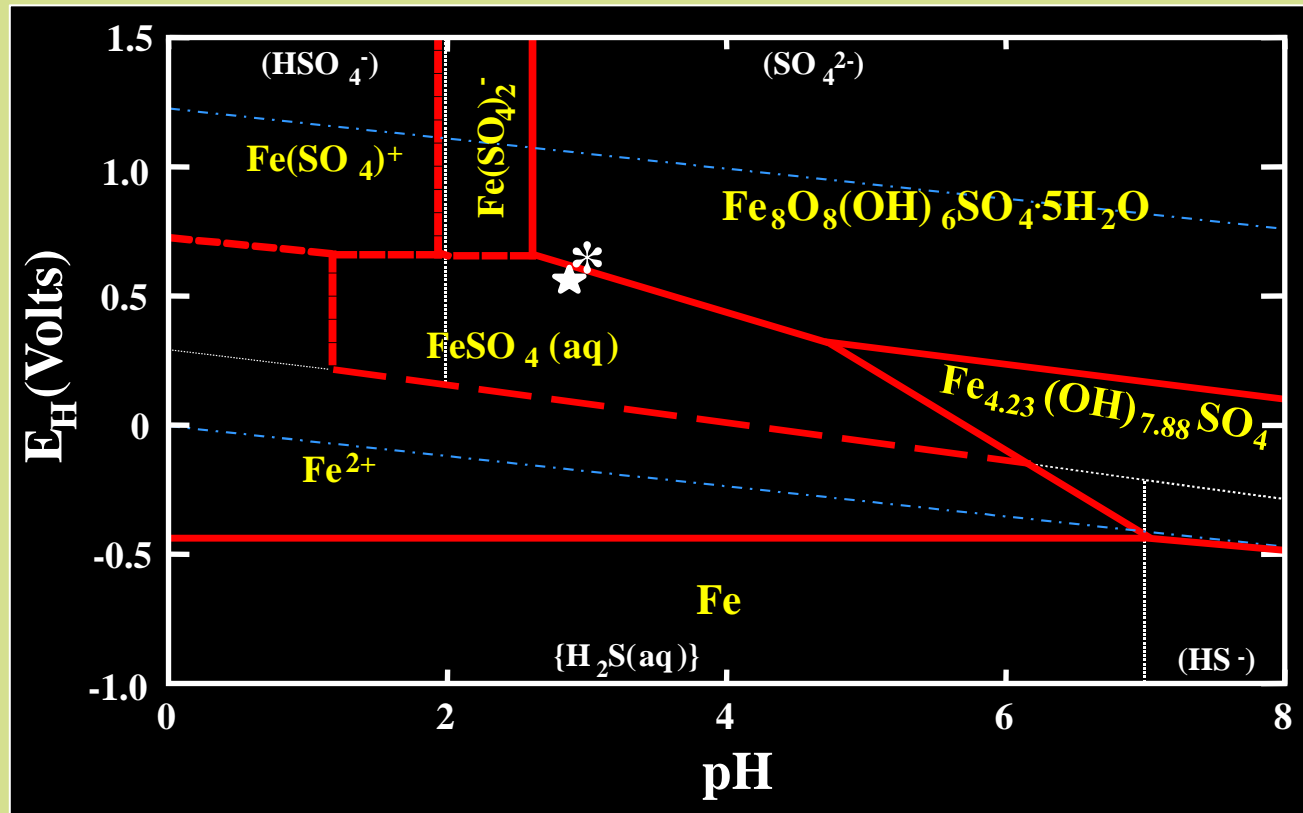


- Selective metal recovery is possible
- **A 7-stage process has been envisioned and shown to work (in batch mode)**
- Fe, As, Cu and Cd met DWS
- **Al almost met DWS**
- Mn and Zn did not meet DWS
- **KMnO₄ addition needs to be precise**
- Zn may have precipitated amorphously
- **SO₄ removal was not done but options are**
 - Freeze Crystallization
 - Reverse Osmosis**
 - Gypsum Precipitation
 - SRB Bioreduction**
 - Chemoreduction
 - Photoreduction**
 - Reductive Precipitation
- **Softening to remove Na, K, Mg and Ca**

Series II – Surface Waters



Series II – Surface Waters



Series II – Surface Waters

- Profiles indicated chemoclines/thermoclines existed and were successfully reproduced in lab
- They have been explained by, but can not be totally attributed to
 - ❖ HSBW being less dense than BPLW so, when it enters the pitlake, it floats on top rather than mixes in, and
 - ❖ Biological activity which should increase DO as well as pH
- Experiments showed that the interaction of sunlight (UV radiation) and air with BPL water plays a significant role

Series III – At Depth

(Deep Water, Pore Water and Sediment)

Collect Core Sample



**Siphon/Filter Off
Deep/Pore Water**



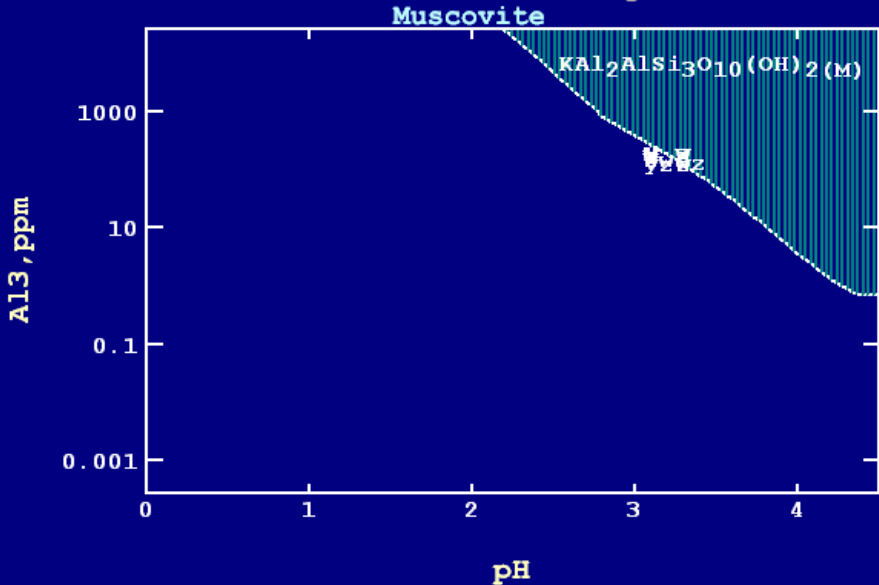
**Analyze the Water
& Solid Contents**

Split & Section the Core

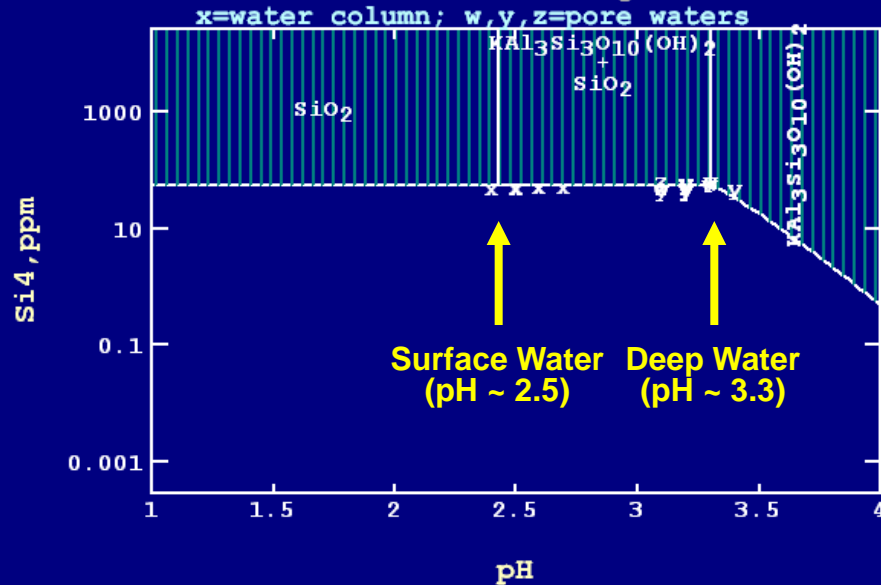


Concentrations are controlled by the solubility of identified minerals and precipitates!

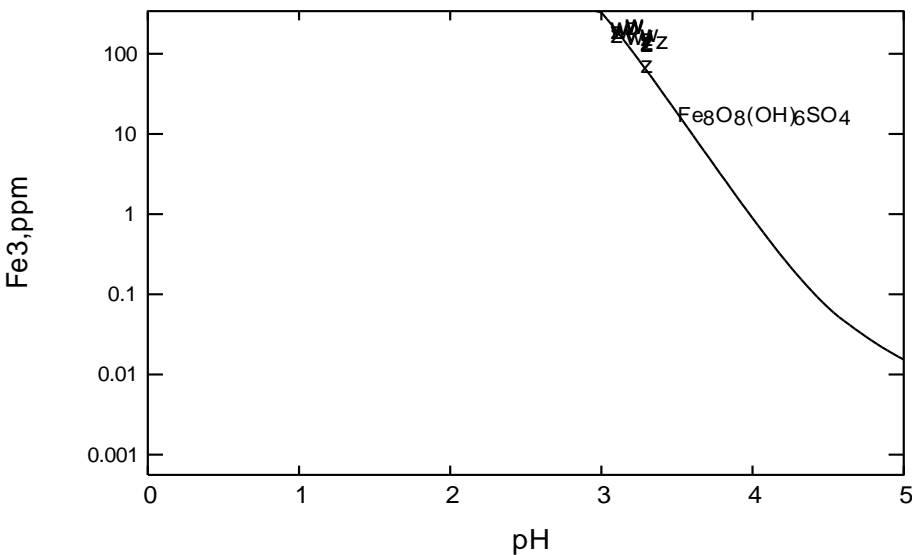
Aluminum Solubility



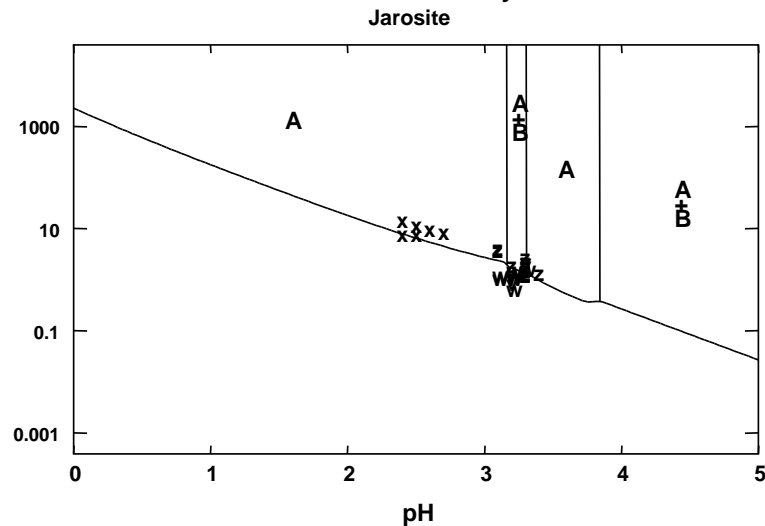
Silicon Solubility



Schwartzmannite



Potassium Solubility



Series III – At Depth

(Deep Water, Pore Water and Sediment)

- Muscovite [$\text{KAl}_3\text{Si}_3\text{O}_{10}(\text{OH})_2$] controls Al^{3+} concentration
- Quartz (SiO_2) controls Si^{4+} concentration
- Schwertmannite [$\text{Fe}_8\text{O}_8(\text{OH})_6\text{SO}_4$] precipitate controls the Fe^{3+} concentration
- Jarosite [$\text{KFe}_3(\text{SO}_4)_2(\text{OH})_6$] precipitate controls K^+ concentration
- Cu^{2+} , Fe^{2+} , Zn^{2+} and Cd^{2+} concentrations could not be associated with a mineral or precipitate are therefore considered to be unsaturated
- However, Cu^{2+} , Fe^{2+} , Zn^{2+} and Cd^{2+} concentrations were found to increase with depth giving the appearance that supergene deposition is occurring

Series IV – Sidewalls

Mineralogy is essentially the same except fine native rock (granite) and gypsum precipitate are more abundant:

Native:

Granite (38%)

Quartz (33%)

Muscovite (4%)

Precipitate:

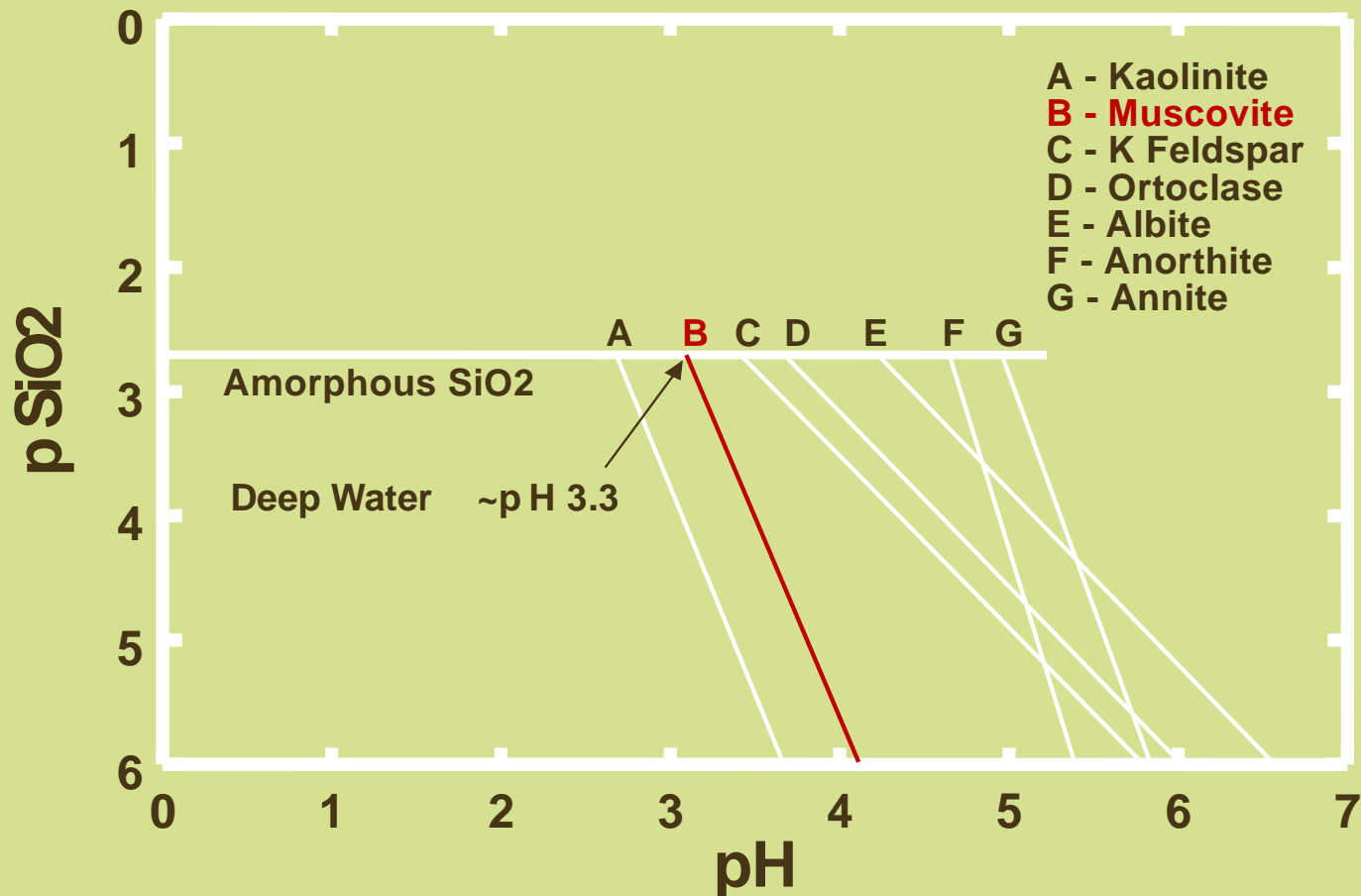
K-jarosite (22%)

Gypsum (3%)



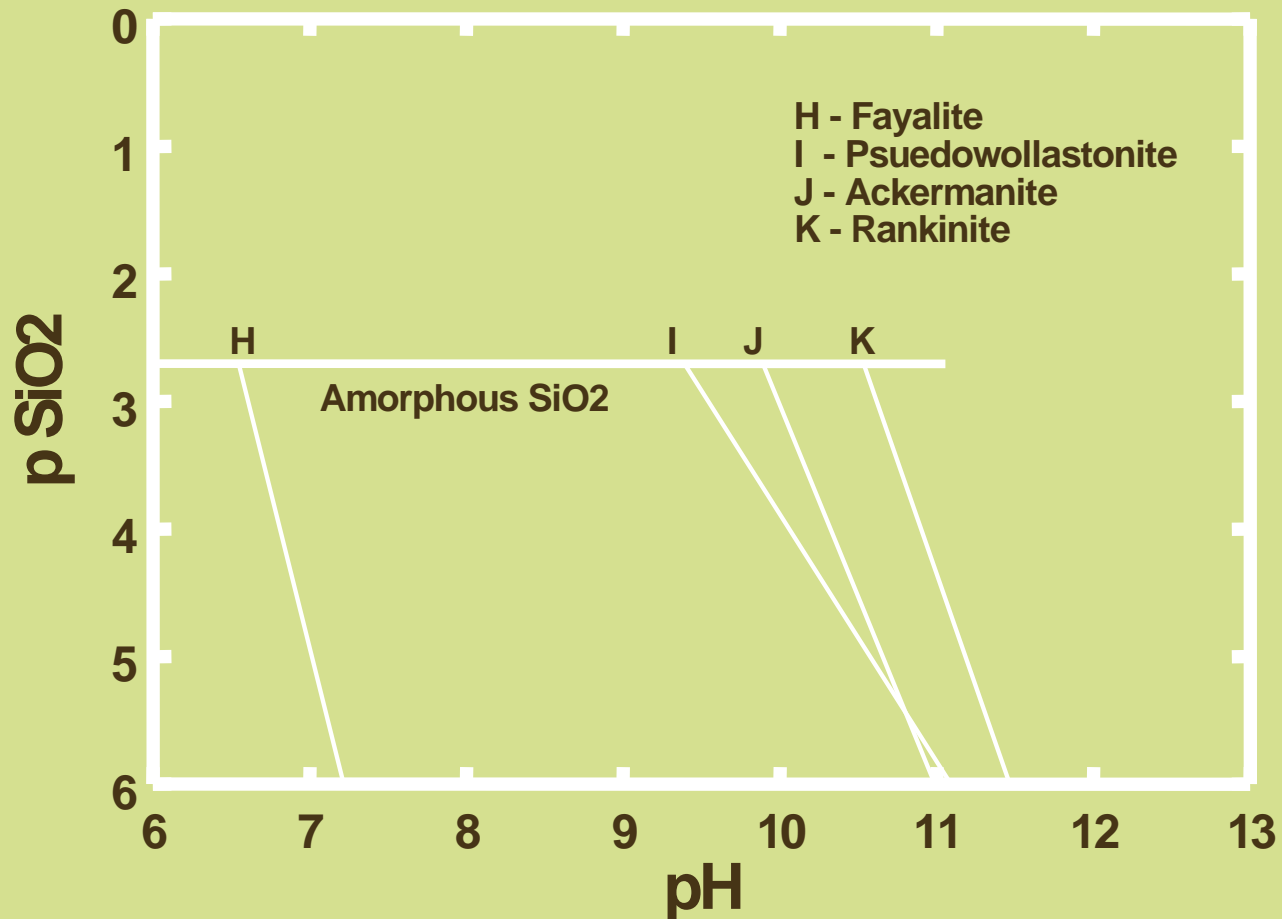
Series IV – Sidewalls

Chemical controls should be about the same as at depth



Series V – Silicate Slags

Silicate (and oxide) slags should do the same thing!



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Silicate Slags

Source of Silicate (and lime)

Act as pH-Buffers (replace lime)

Available in Montana (inactive)

Anaconda (ARCO) - Fayalite, Fe_2SiO_4

East Helena (ASARCO) - Olivine-type, CaFeSiO_4

Rocker (Rhone) - Pseudowallastonite, CaSiO_3

Slag	Ca (%)	Fe (%)	Si (%)
Rhone	30.3	0.4	19.0
ASARCO	14.0	27.6	12.7
Anaconda	2.6	30.9	15.8

Silicate Slags

Other Global Sources

Columbus (Stillwater)

Salt Lake City (Kennecott)

Trail, BC (Teck Cominco)

Dual Ecosystem Enhancement

Remove Slag Piles

Remediate Berkeley Pitlake

In-Situ or Ex-Situ

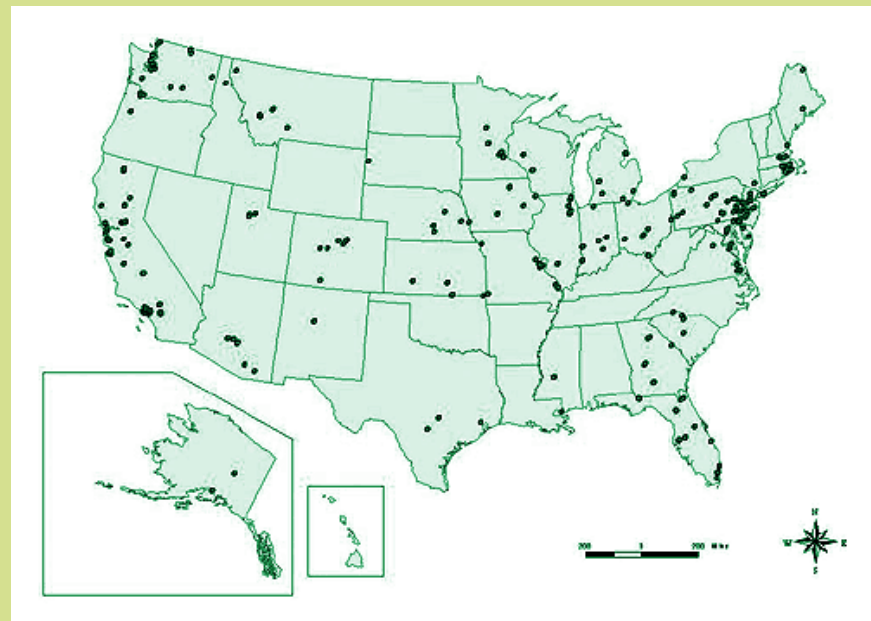
Provide Entertainment

Golf Courses

Parks & Walkways

Sports Complexes

Attract Businesses



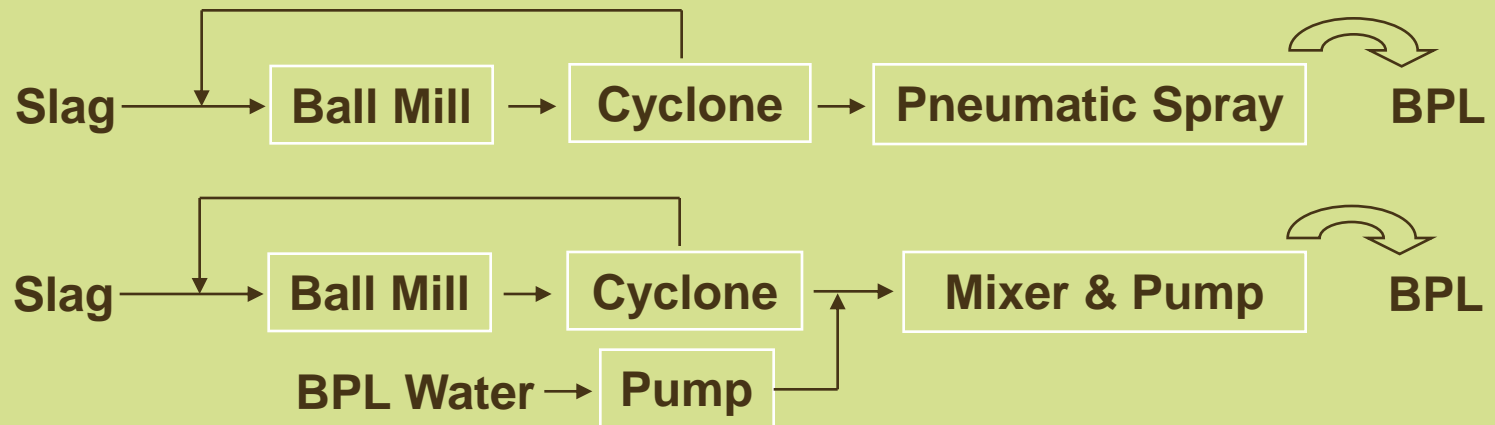
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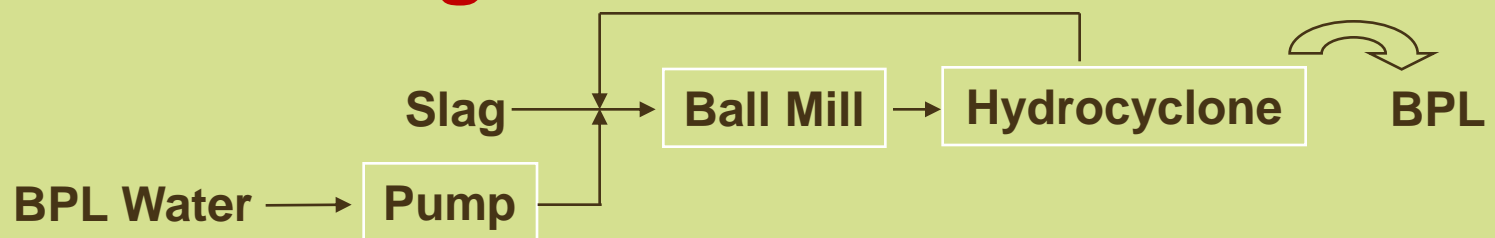
Objectives

Conceptual Flowsheet Designs

Dry Grinding



Wet Grinding



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Procedures

Characterize Montana Slags

Bond Work Index

SEM/EDX/MLA Analysis

Remediation Potential

Model Effects

Parameters

Slag Type (Fe/Si Ratio)

Particle Size (100-400 Mesh)

Slag Amount (200-800 g/L)

Experimental Design (StatEase)

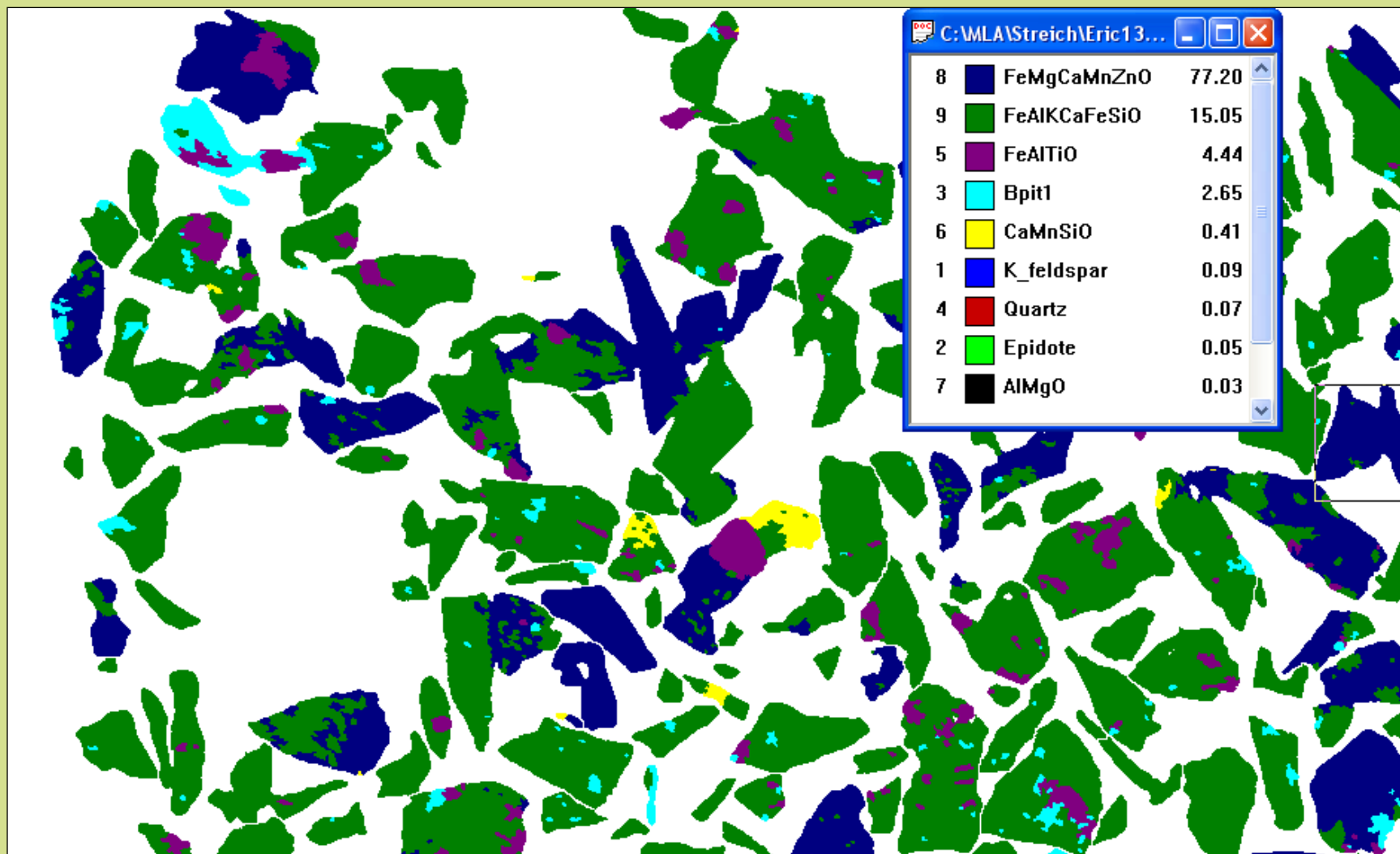
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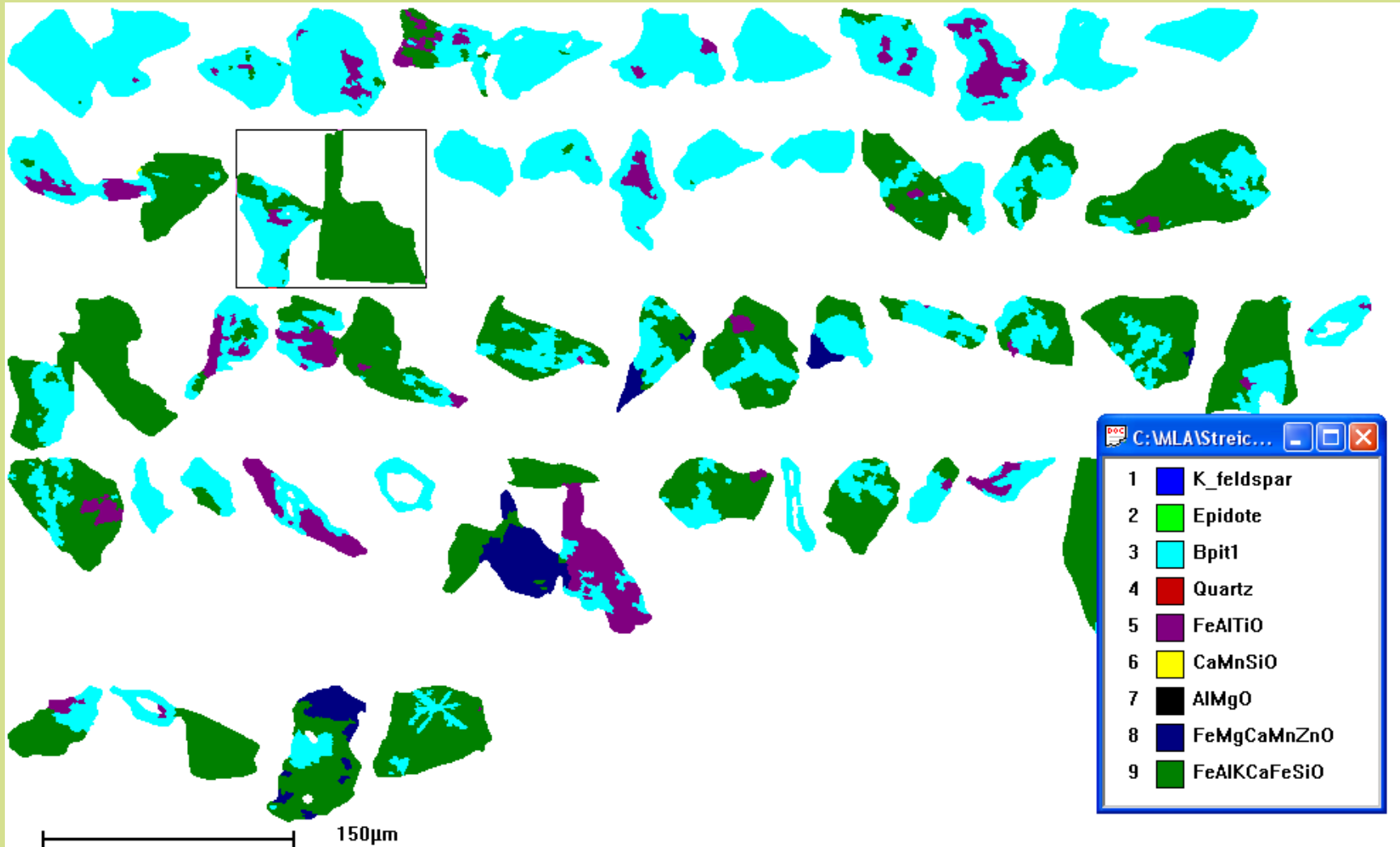
Bond Work Index

Date	Slag	Target Size Mesh (mm)	F80 (mm)	P80 (mm)	Avg Gbp	Bond Work Index
1/29/05	ACC	48 (0.295)	2.825	0.205	0.95	20.52
2/17/05	ACC	100 (0.147)	2.603	0.117	0.94	20.44
2/20/05	ACC	200 (0.074)	2.603	0.058	0.53	24.86
1/29/05	ASARCO	48 (0.295)	2.652	0.230	1.76	16.26
2/12/05	ASARCO	100 (0.147)	2.555	0.113	1.24	15.93
1/30/05	ASARCO	200 (0.074)	2.603	0.053	0.50	24.68
2/26/05	RP	48 (0.295)	1.414	0.251	2.79	14.18
3/4/05	RP	100 (0.147)	1.414	0.121	1.53	15.48
3/4/05	RP	200 (0.074)	1.414	0.063	0.76	20.66

SEM/EDX/MLA Analysis (150 um Asarco Slag Before)

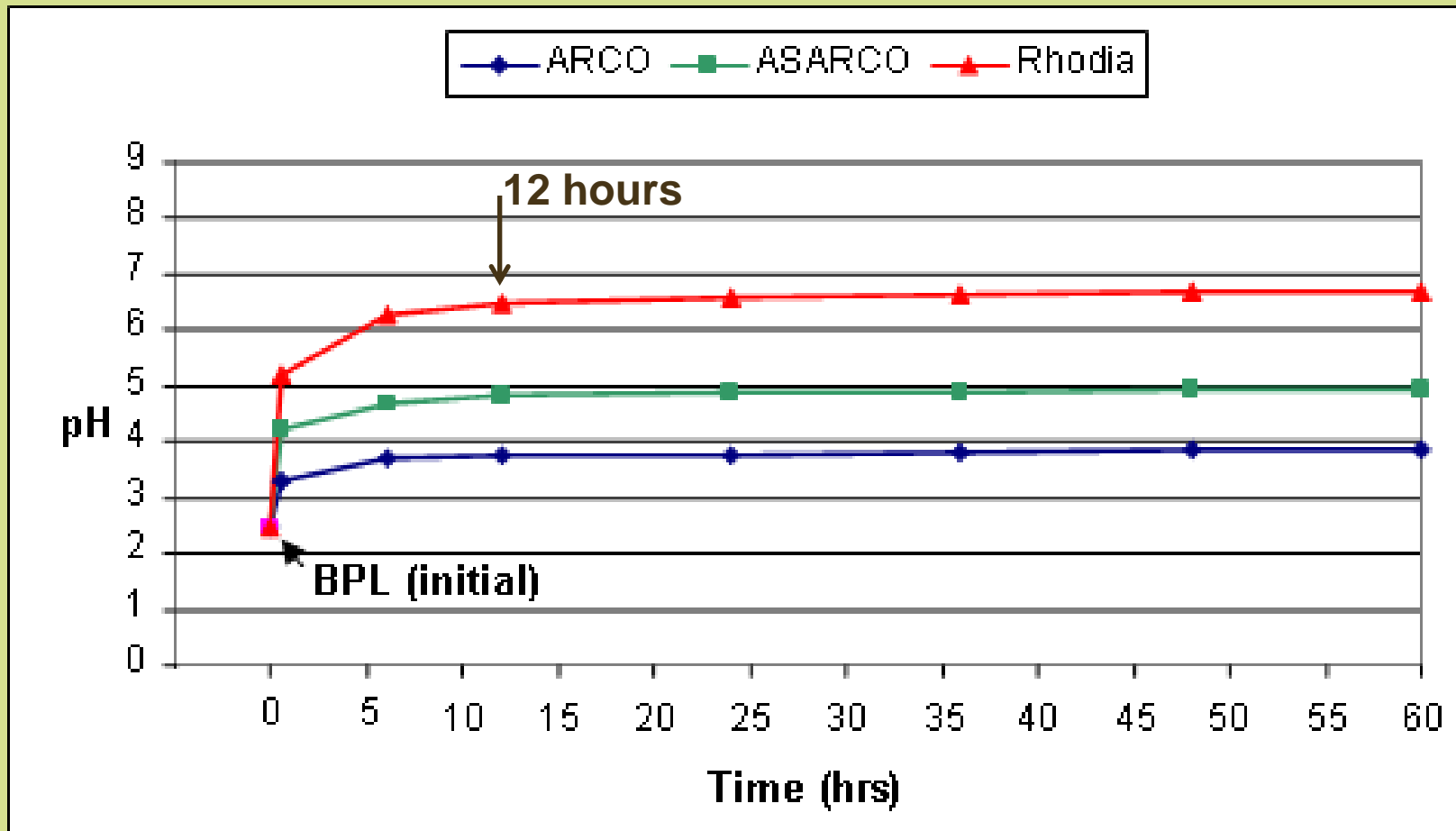


SEM/EDX/MLA Analysis (150 um Asarco Slag After)



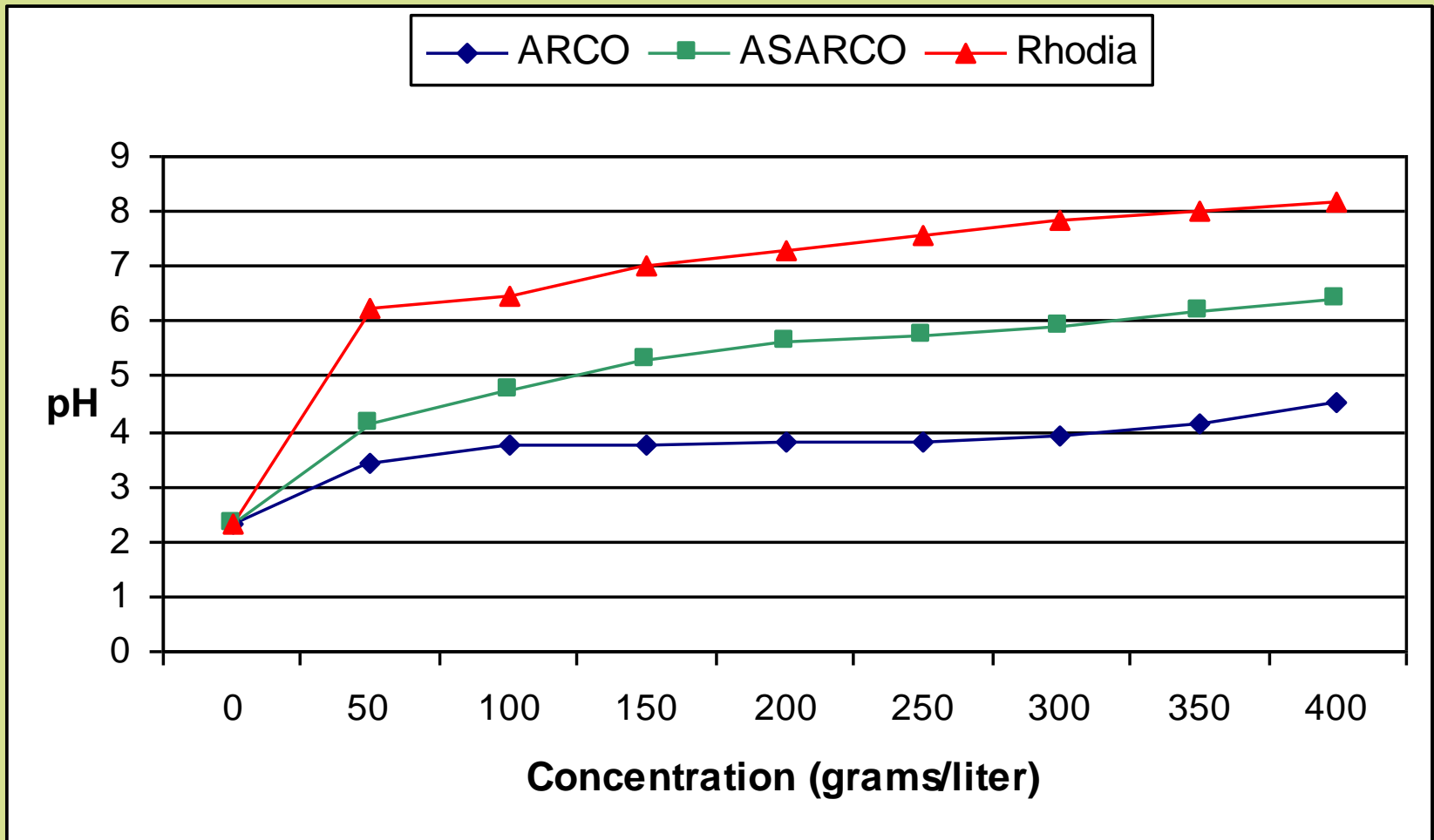
Remediation Potential (Bottle Roll Tests)

Size = 53 μm ; Amount = 100 g/L



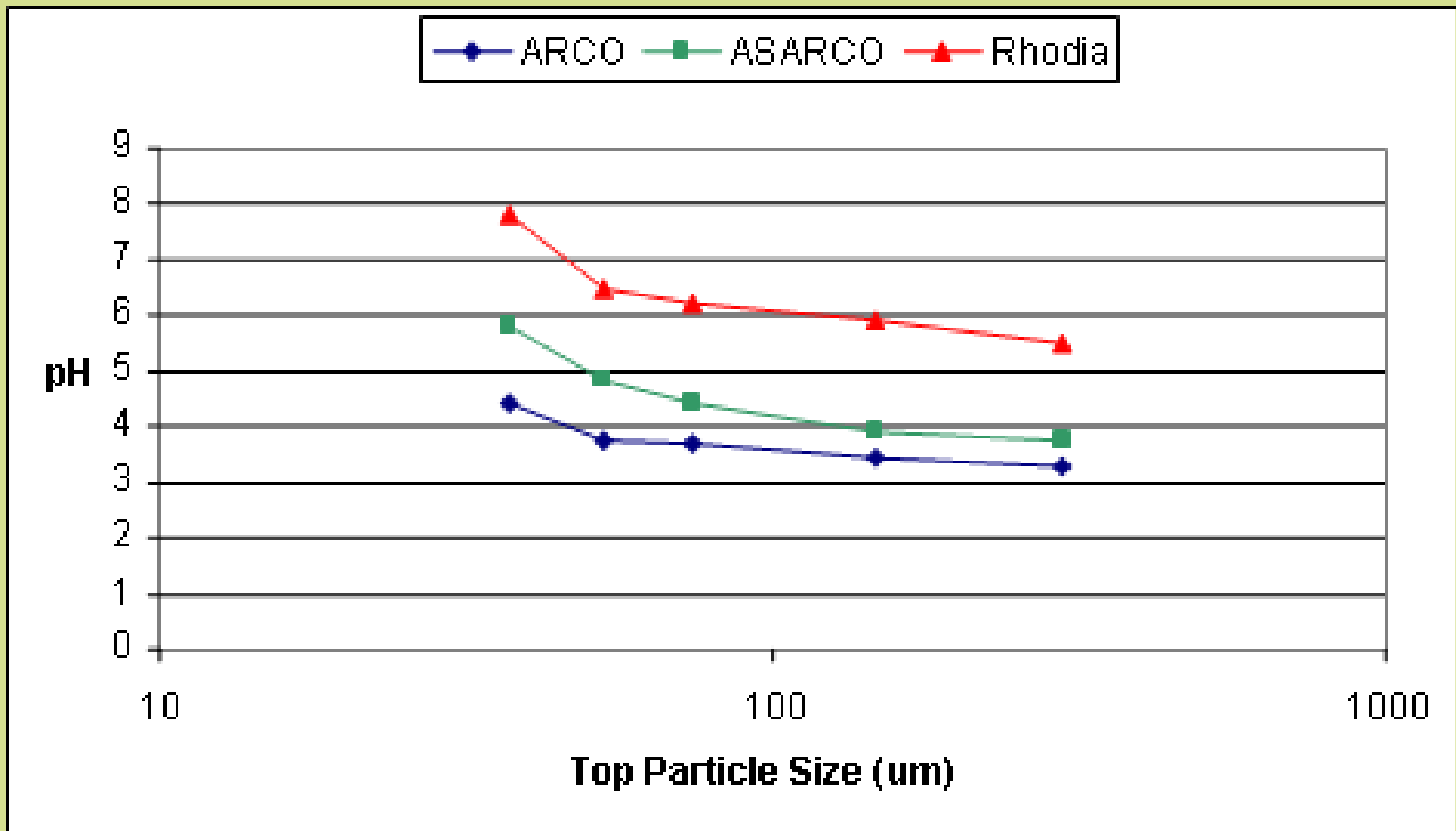
Remediation Potential (Bottle Roll Tests)

Size = 53 μm ; Time = 12 hrs



Remediation Potential (Bottle Roll Tests)

Amount = 100 g/L; Time = 12 hrs



StatEase Design of Experiments (Box-Behnken Matrix)

Run	Slag Type (Fe/Si Ratio)	Particle Size (μm)	Slag Amount (g/L)
1	0 = Rhodia	-37 = 400 mesh	500
2	2 = ARCO	-37	500
3	0	-147 = 100 mesh	500
4	2	-147	500
5	0	-74 = 200 mesh	200
6	2	-74	200
7	0	-74	800
8	2	-74	800
9	1 = ASARCO	-37	200
10	1	-147	200
11	1	-37	800
12	1	-147	800
13	1	-74	500
14	1	-74	500
15	1	-74	500

	pH	Al	As	Cd	Cu	Fe	Mn	SO ₄ ²⁻	Zn
Test Run	BPL Concentrations (mg/L)								
	2.5	289	0.15	2.1	168	793	276	2723	621
	Final Responses (mg/L)								
1	9.08	0.043	0.0025	0.002	0.19	0.29	4.42	829	0.24
2	5	6.32	0.09	2.1	2.26	95	276	1980	621
3	7.77	0.20	0.001	0.034	0.063	0.069	57.8	1075	2.02
4	5.19	11.6	0.09	1.69	34.2	772	276	2210	621
5	7.68	0.20	0.0008	0.055	0.136	0.096	83.7	619	3.84
6	4.55	37.8	0.15	2.1	168	793	268	2450	621
7	8.42	0.041	0.001	0.002	0.179	0.014	5.13	879	0.11
8	5.52	0.37	0.039	1.13	0.566	271	276	1720	531
9	5.62	1.39	0.0049	1.03	0.39	6.99	266	1680	601
10	4.74	26.1	0.021	1.57	18.05	595	265	2045	621
11	6.89	0.20	0.0014	0.059	0.095	0.069	181	1270	24.1
12	6.16	0.444	0.0023	0.38	0.141	2.37	248	1395	212
13	6.02	0.62	0.0023	0.44	0.174	4.77	250	1410	278
14	6.08	0.53	0.0023	0.42	0.139	3.76	248	1410	254
15	6.08	0.51	0.0022	0.45	0.277	3.67	252	1450	257
	Drinking Water Standards (mg/L)								
	6.5 - 8.5	0.05	0.01	0.005	1.3	0.3	0.05	250	5

StatEase Model Equations

A = Fe/Si Ratio (0-2); B = Size (um); C = Amount (g/L)

$$\text{pH} = 8.31 - 3.49A - 0.0012B + 0.0018C + 0.006AB + 0.7A^2$$

$$\text{Log [H]} = -8.31 + 3.49A + 0.0012B - 0.0018C - 0.006AB - 0.7A^2$$

$$\text{Log [Al]} = 2.05 + 1.44A + 0.0063B - 0.0011C - 0.0011AC$$

$$[\text{As}]^{0.5} = 0.39 + 0.48A + 0.0015C - 0.006AC + 3.35A^2$$

$$[\text{Cd}]^{0.5} = 16.77 + 20.36A - 0.027C$$

$$\text{Log [Cu]} = 2.29 + 0.17A + 0.0074B - 0.0019C + 0.0083AB - \\ 0.0023AC - 0.00002BC + 0.59A^2 + 0.0000038C^2$$

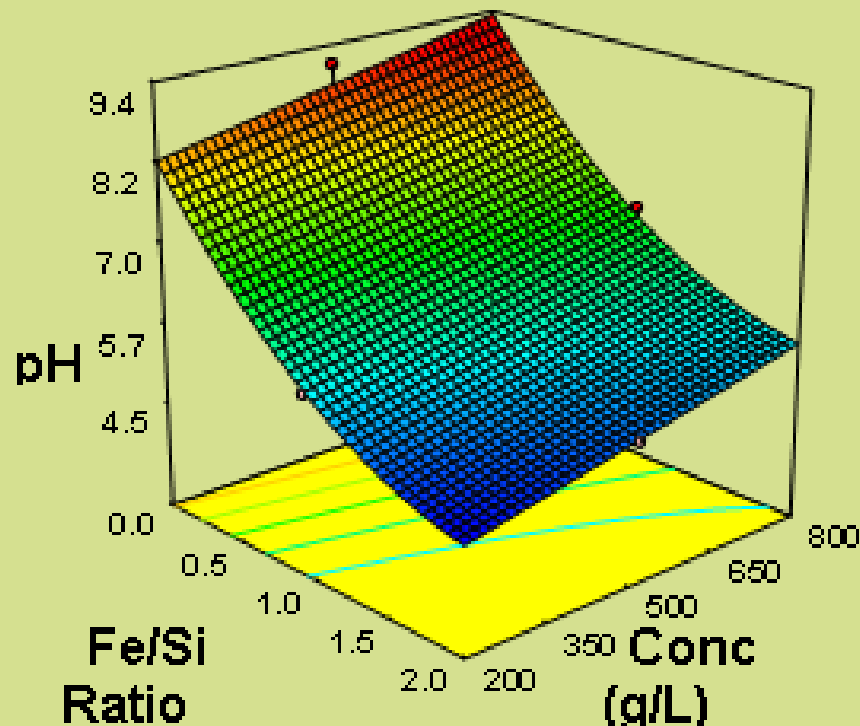
$$\text{Log [Fe]} = 2.1 + 1.95A + 0.0099B - 0.0025C$$

$$[\text{Mn}] = 738886 + 26555A + 252B - 127C + 63.5AC - 86310A^2$$

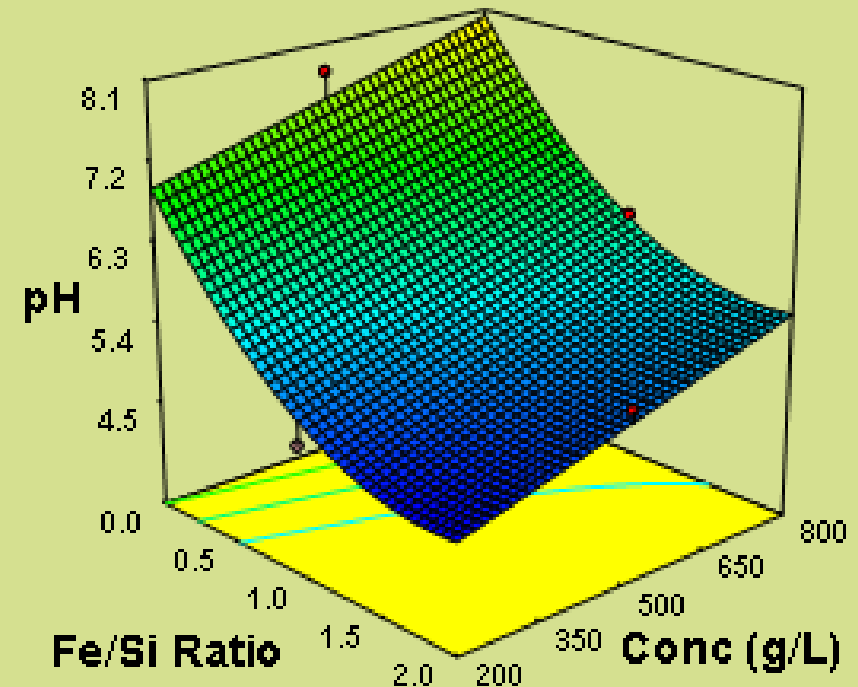
$$[\text{Zn}]^{0.5} = 315.4 + 420A - 0.49C$$

StatEase Model Plots

Size = 37 μm



Size = 147 μm



StatEase Model Plots

Design-Expert® Software

pH

10.05

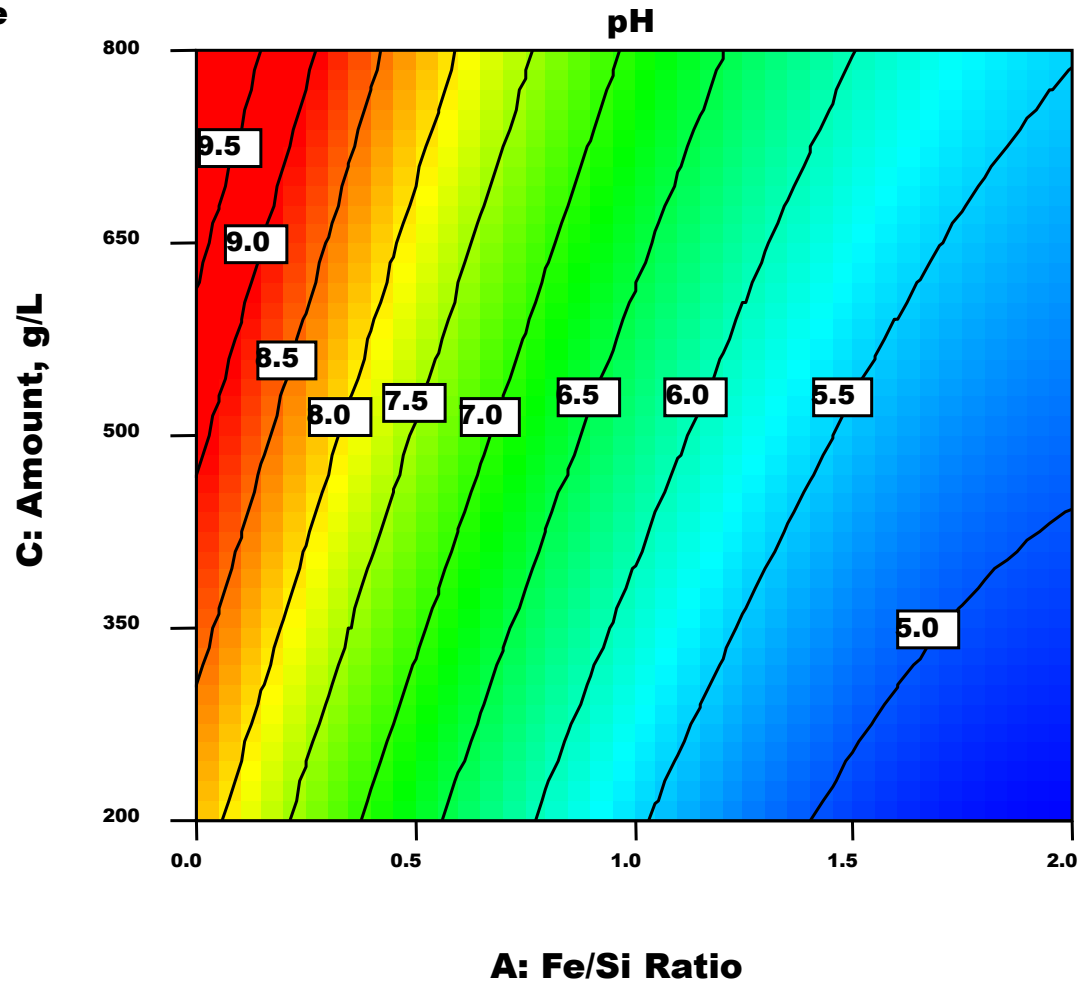
4.57

X1 = A: Fe/Si Ratio

X2 = C: Amount, g/L

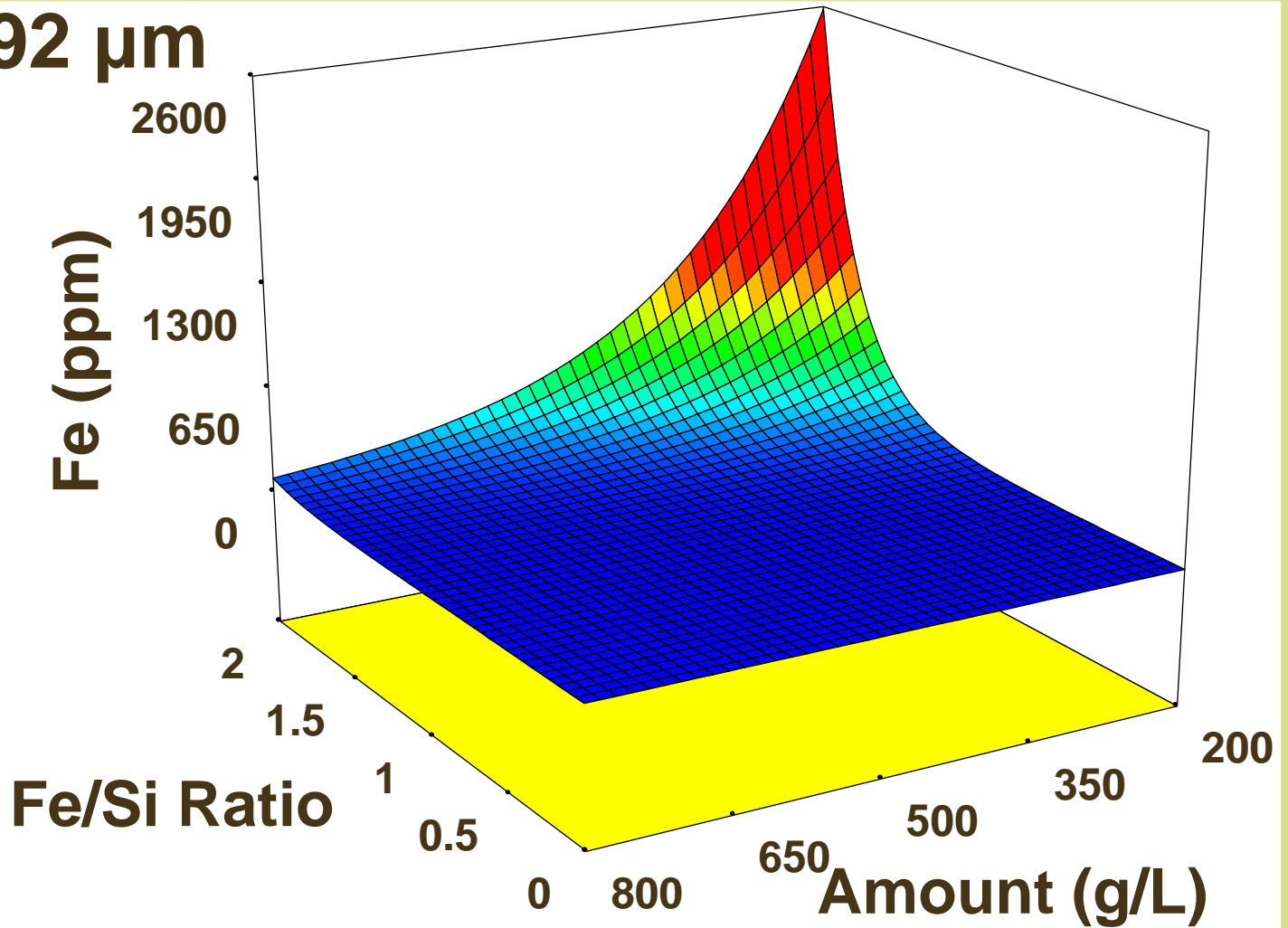
Actual Factor

B: Size, $\mu\text{m} = 37$



StatEase Model Plots

Size = 92 μm



StatEase Model Plots

Design-Expert® Software

Original Scale

Log10(Fe, ug/L)

974000

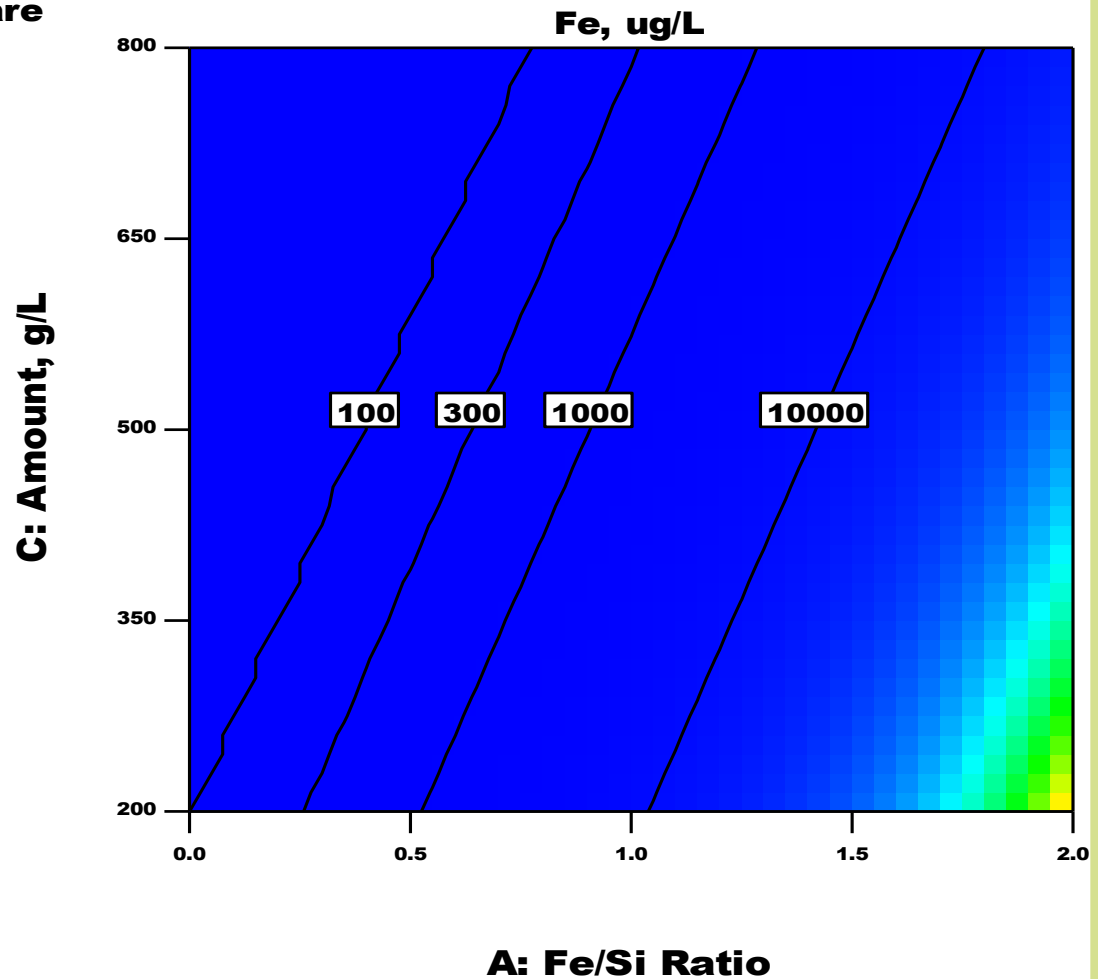
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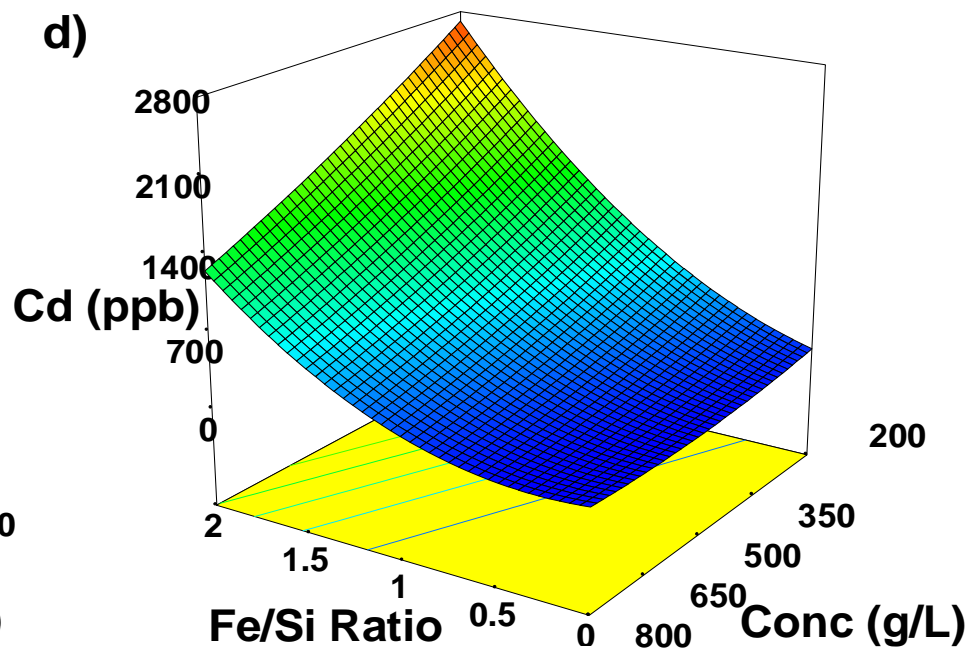
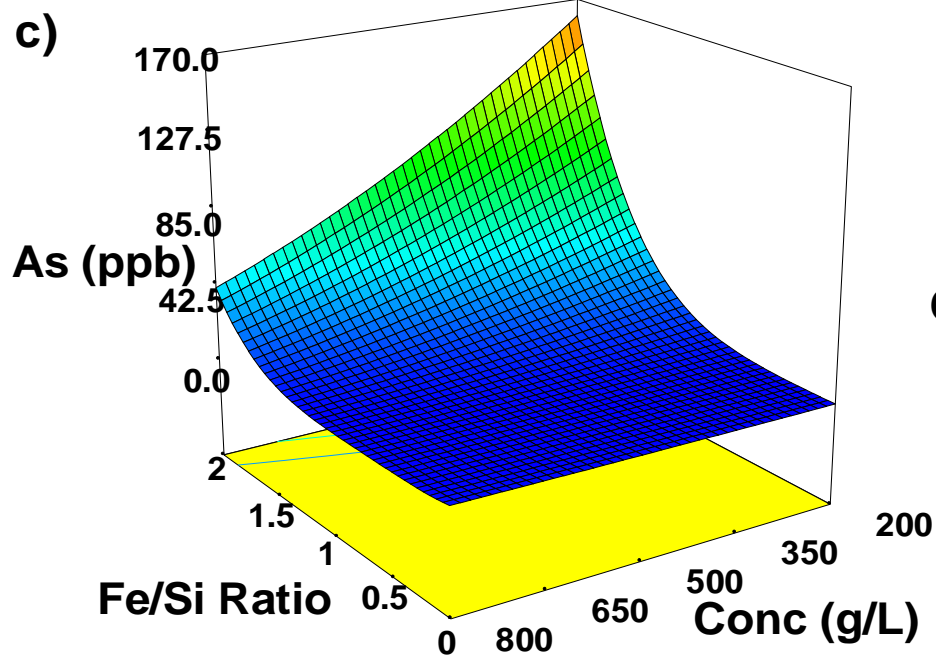
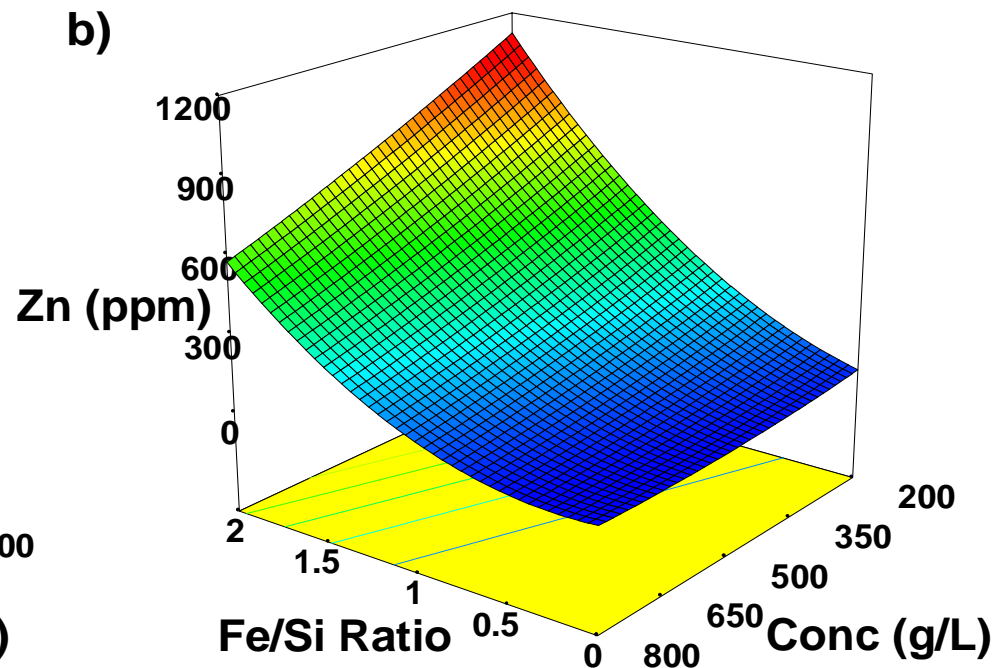
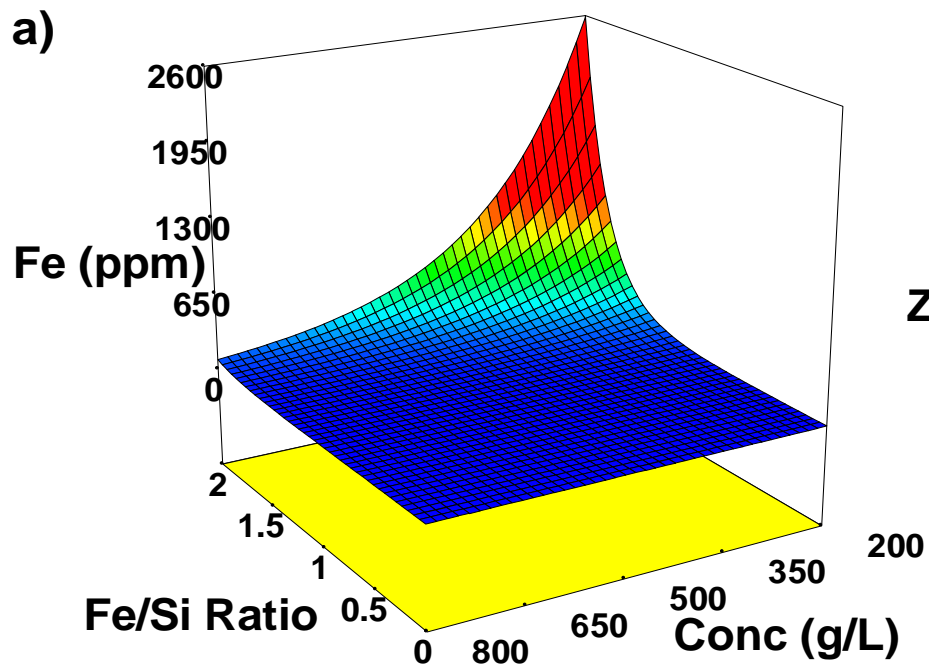
X1 = A: Fe/Si Ratio

X2 = C: Amount, g/L

Actual Factor

B: Size, um = 37





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Conclusions

- ✓ Slags can be an effective for remediating ARD
- ✓ **Their use could or will:**
 - replace lime (pseudowollastonite slag)
 - diminish lime consumption (fayalite/olivine)**
 - lead to remediation of two ecosystems
- ✓ **Depending on the slag type and particle size:**
 - effluent pH from 5-9 can result
 - effluent concentrations can meet DWS**
- ✓ Al and Cu concentration profiles are similar to Fe
- ✓ **Likewise, Al and Cu redissolution at high pH is minimal similar to Fe**

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Acknowledgements

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We are always on the lookout for funding Series VI to ∞!

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Thanks For Your Attention!



**U.S. EPA Hardrock Mining Conference
(Advancing Solutions for a New Legacy)
Denver CO April 3-5, 2012**



